Bailieboro Foods Ltd. and Bailie Foods Ireland Ltd. Application for an IPPC Licence Review



1.0 Operational Information Requirements

1.1 Development and Operational History of the Site

The following sets out the development and operational history of the plant.

- **1902** Bailieboro Co-op formed.
- **1965** Evaporator was built on Bailieboro site by MacCormac's (Prictchitts) and Engineering business.
- 1973 The evaporator became a joint venture with Bailieboro Co-op.
- **1979** Spray drier (Bailie Foods), water and effluent treatment plant were built.
- **1981** Spray drier was replaced and comissioned for Fat filled powder.
- 1985 Feta cheese factory and engineeering offices were built.
- **1986** New milk intake and water treatment plant was erected.
- **1988** Entire business was sold to Food Industries leading to the closure of the cheese plant and the sale of Engineering works.
- **1989** The Evaporator was upgraded to facilitate the evaporation of high heat heat stable products and in the powder plant a final single effect evaporator (Finisher) was installed and the Fluidized Bed was replaced to incorporate a well mix section. Improved product output.
- **1990** Golden Vale Plc. purchased from Food Industries the Bailieboro milk division.
- **1992** A bulk powder tanker and mini bulk filling system was installed and the boilers were converted to natural gas.
- **2000** Bailieboro Foods Ltd. and Bailie Foods Ireland Ltd was granted an IPC licence (Reg. No. 406) under section 83(1) of the Environmental Protection Agency Act, 1992
- **2001** A washable Bag Filter system was installed which reduced our particulate emissions to less than 10 mgs per m3.
- 2001 Golden Vale PLC was taken over by Kerry Group PLC in 2001.
- 2002 Lakeland Dairies purchased the Bailieboro Milk Division from Kerry Group PLC.
- **2006** A review of the licence was granted (IPPCL Reg. No. 406-02) for the installation of a Combined Heat and Power Plant with a new emission to air point and for the installation of an Integrated Constructed Wetland (ICW) to treat wastewaters arising at the plant prior to discharge to the River Lear by a new emission point.
- **2010** A new additional dryer is expected to be commissioned in April 2010 at the facility subject to EPA approval.

2.0 Operational Information: Proposed Upgrades

2.1 Milk Intake

The milk intake area will be upgraded to increase storage capacity as very low storage capacity has been a problem in the past. A layout of the milk intake process with the new proposed tanks is enclosed with this Attachment (Figure 9. Proposed additional tank locations).

Whole Milk Storage

The current design includes the installation of 2 additional whole milk storage silos, each with a volume of 250,000 litres. There are 4 existing silos each with a capacity of 110,000 litres. The total whole milk storage capacity will therefore be 890,000 litres.

Separation/Pasteurisation

One new separation stream is to be installed and will have a capacity of 50,000 litres/hour (replacing an existing stream with a capacity of 25,000 litres/hour). Two existing separation streams will remain, one with a capacity of 32,000 litres/hour and the other at 25,000 litres/hour. Therefore the total processing capacity will be 107,000 litres/hour.

Processed Milk Storage

There are 5 existing processed (skim) milk silos. 4 of the silos have a capacity of 110,000 litres and the 5th has a capacity of 180,000 litres. It is planned to install 3 additional silos (dedicated to the new evaporator/dryer process) each with a capacity of 250,000 litres. The total storage volume will therefore be 1,370,000 litres.

Cream Handling

Additional plates will be added to an existing crean pasteuriser and the other existing pasteuriser will be replaced to give the planned flexibility and capacity. There should be limited overall increase in cream handling operations.

2.2 Drying process: New proposed dryer

The spray drying plant is designed for drying of whole milk, buttermilk and skim milk to produce an agglomerated powder at a capacity of approx. 7,000 kg/h of final dried instant whole milk powder. The potential capacity on skim milk powder is 6,300 kg/h. The concentrate to be dried is pumped from the evaporator through a filter, by means of a centrifugal pump, and to the nozzle unit by means of a high-pressure pump with homogenizer. The drying air is passed through air filters and heated in an indirect steamheated air heater and an indirect gas-heated booster before entering a specially designed air disperser. An operational flowchart is enclosed with this attachment.

The exhaust air is discharged through a new emission point (A27) from the ceiling of the drying chamber and is passed through a high-efficient bag filter for collection of powder entrained in the air. The bag filter is in a sanitary design, and it can be wet Cleaning In Place (CIP) cleaned. The fines fraction is returned to the drying chamber or the VIBRO-FLUIDIZER® for obtaining the desired agglomeration degree. The drying chamber is equipped with an integrated fluid bed for a lenient secondary drying and agglomeration, in order to improve the final product quality and drying economy. The powder is finally dried and cooled in a VIBRO-FLUIDIZER® before sieving and bagging off. For production of instant whole milk, a lecithination unit has been included. The technology includes a safety system, independent of the CIP equipment. The evaporator and spray dryer operation is fully automated inclusive of start-up and shut-down procedures ensuring optimal performance and minimal product loss and down time.

Cleaning takes place by means of lye followed by flushes of water, acid and caustic soda. A new CIP plant with two new 12m³tanks will be installed. The CIP plant will be bunded in accordance with EPA guidelines 'Storage and Transfer of Materials for Scheduled Activities' (2004).

The heat recovery system utilises the hot condensate from the evaporator. Some of the hot condensate from the evaporator is used to preheat the incoming feed. The hot condensate not used for preheating the feed is used to preheat the air for the spray dryer.

The new dryer is to be installed adjacent to the existing dryer in the current storage area. The majority of the new development will be within the existing building footprint. Figure 1 in Attachment D shows the location of the proposed changes to the existing building footprint within the context of the overall site. The new dryer will be controlled from a common control room within the existing plant. A new set of locker rooms and changing rooms will be provided to segregate the store, wet and dry areas. It is planned to install a new powder packing line adjacent to the existing one. The existing ground floor layout and proposed layout is shown in figures 2 and 2a (Attachment D). Figures 3 and 4 (Attachment D) show the elevation of the proposed dryer building. Figure 5 (Attachment D) shows the location of the proposed new dryer emission to air point on the roof. Figure 6 shows all the air emission points applicable to the licence review including the existing and new dryer emission points. The coordinates of the new dryer emission point are 267,795E 298,045N.

3.0 Existing emission points A1-5 (Boiler) A1-6 (Boiler) and A25 (CHP plant)

A review of the IPPC licence was carried out in 2006. At the time the EPA approved the operation of the CHP plant (A25) and the licence was amended. The changes to the licence in 2006 in order to accommodate the CHP plant were sufficient to support existing operations. Scheduled B1 of the licence set out the emission limit values for the CHP plant (A 25) and boilers (A1-1, A1-2, A1-5, A1-6) and stated that A1-5 had to be decommissioned prior to installation of the CHP plant.

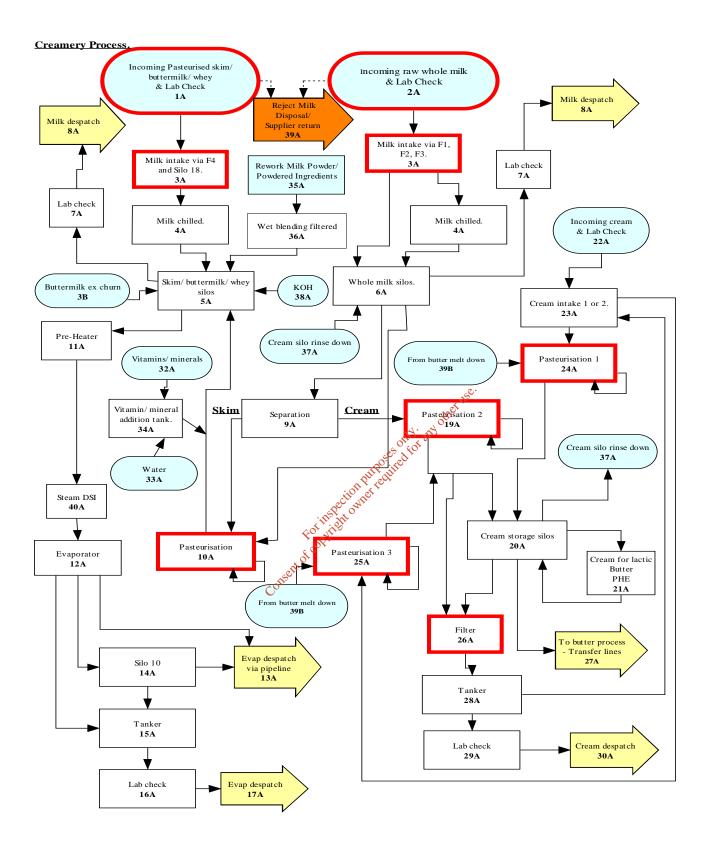
Following a review of the energy requirements to facilitate the installation of the new dryer and increase the capacity of the plant, it has been concluded that four boilers (emission points A1-1, A1-2, A1-5 and A1-6) will be required to run both dryers simultaneously in the event of a malfunction of the CHP plant.

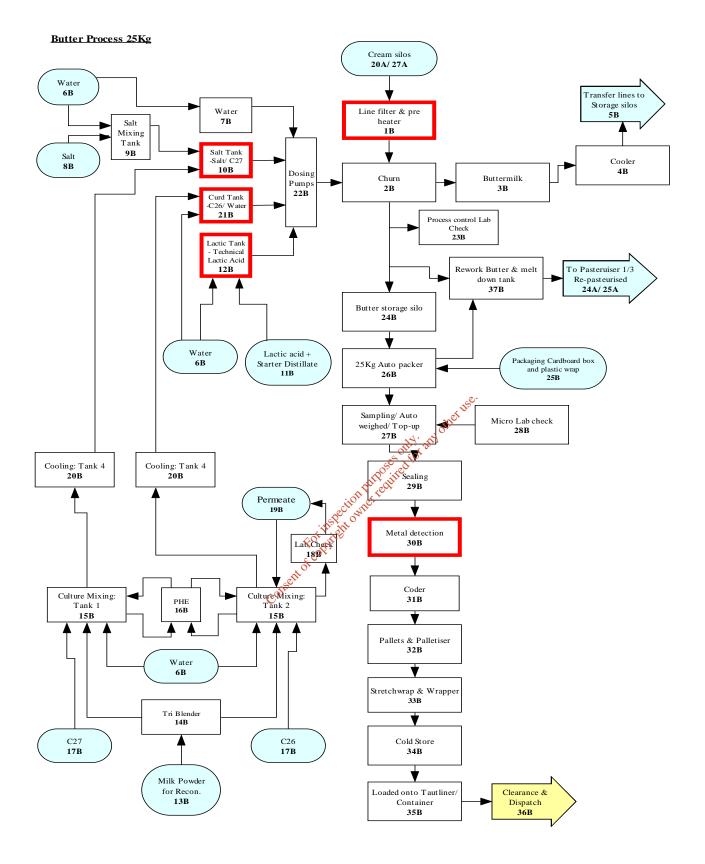
Since the last review, the location of the CHP plant has been revised. The revised coordinates of the CHP emission point are E267804 N297972.

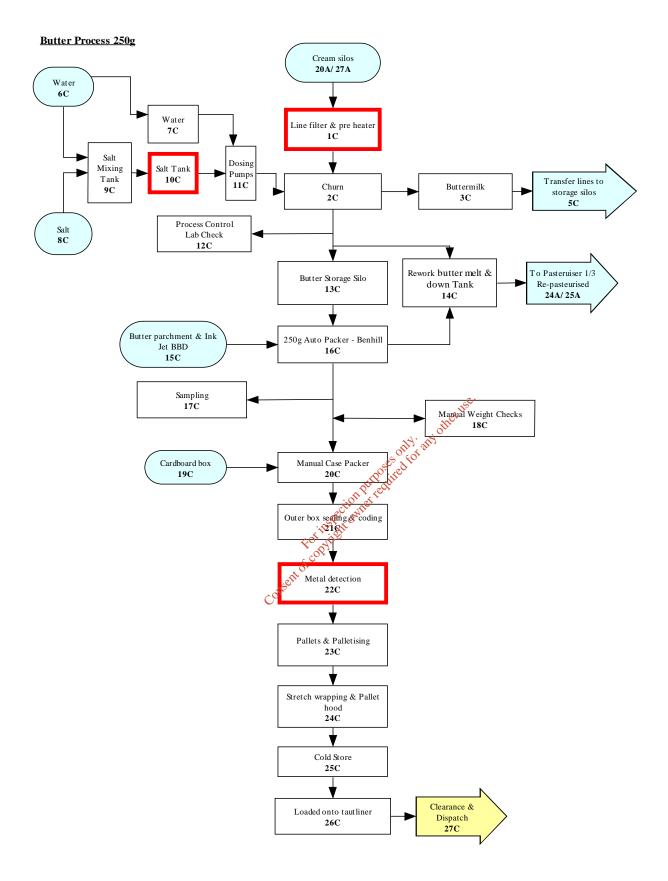
Figure 8 (Attachment D) shows the location of the boilers and CHP plant. Figure 6 and 7 (Attachment D) shows the location of the boiler (A1-1, A1-2, A1-5 and A1-6) and CHP (A25) emission points.

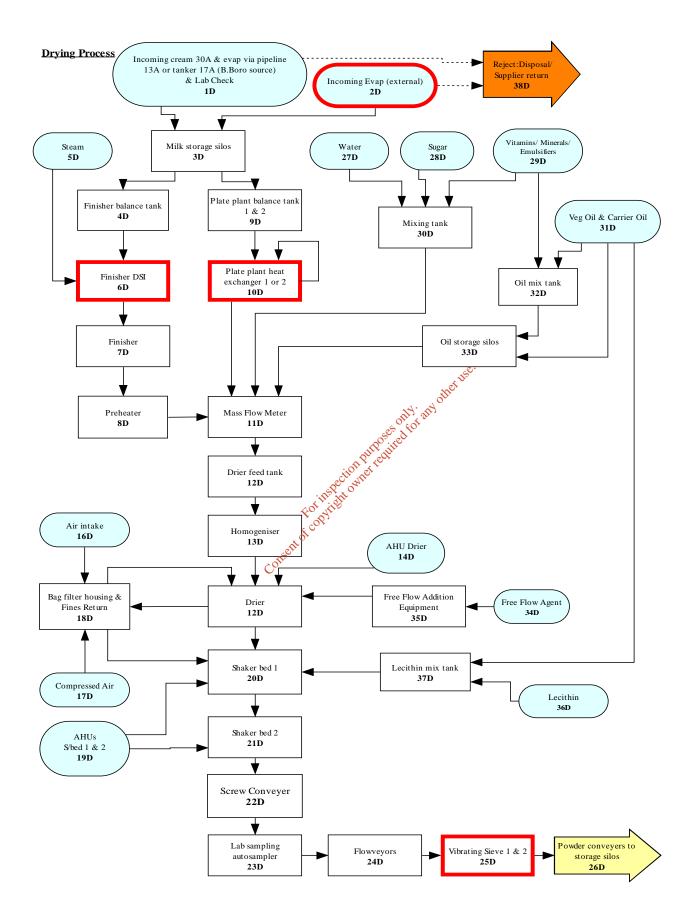
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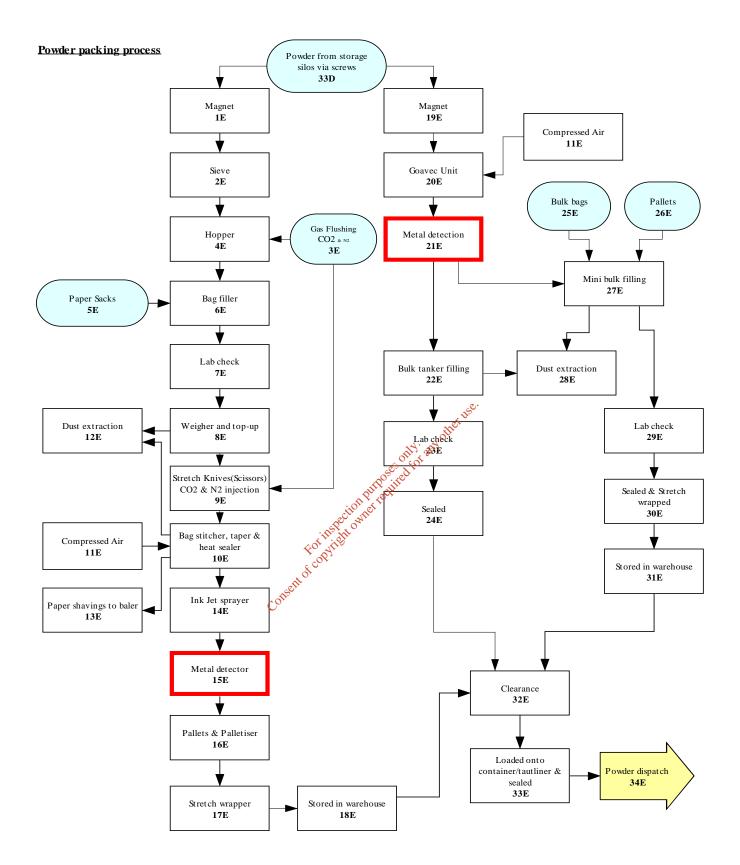










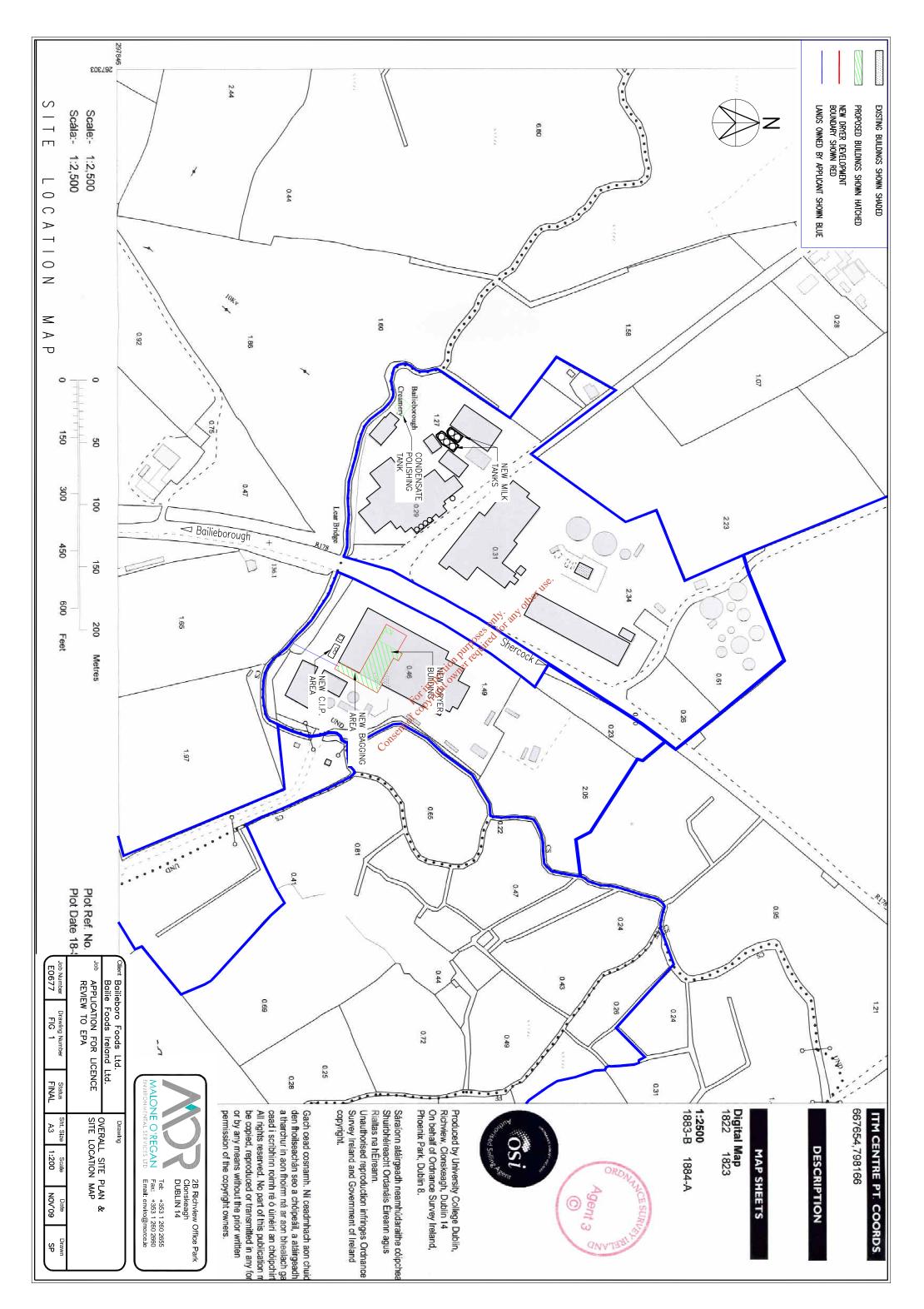


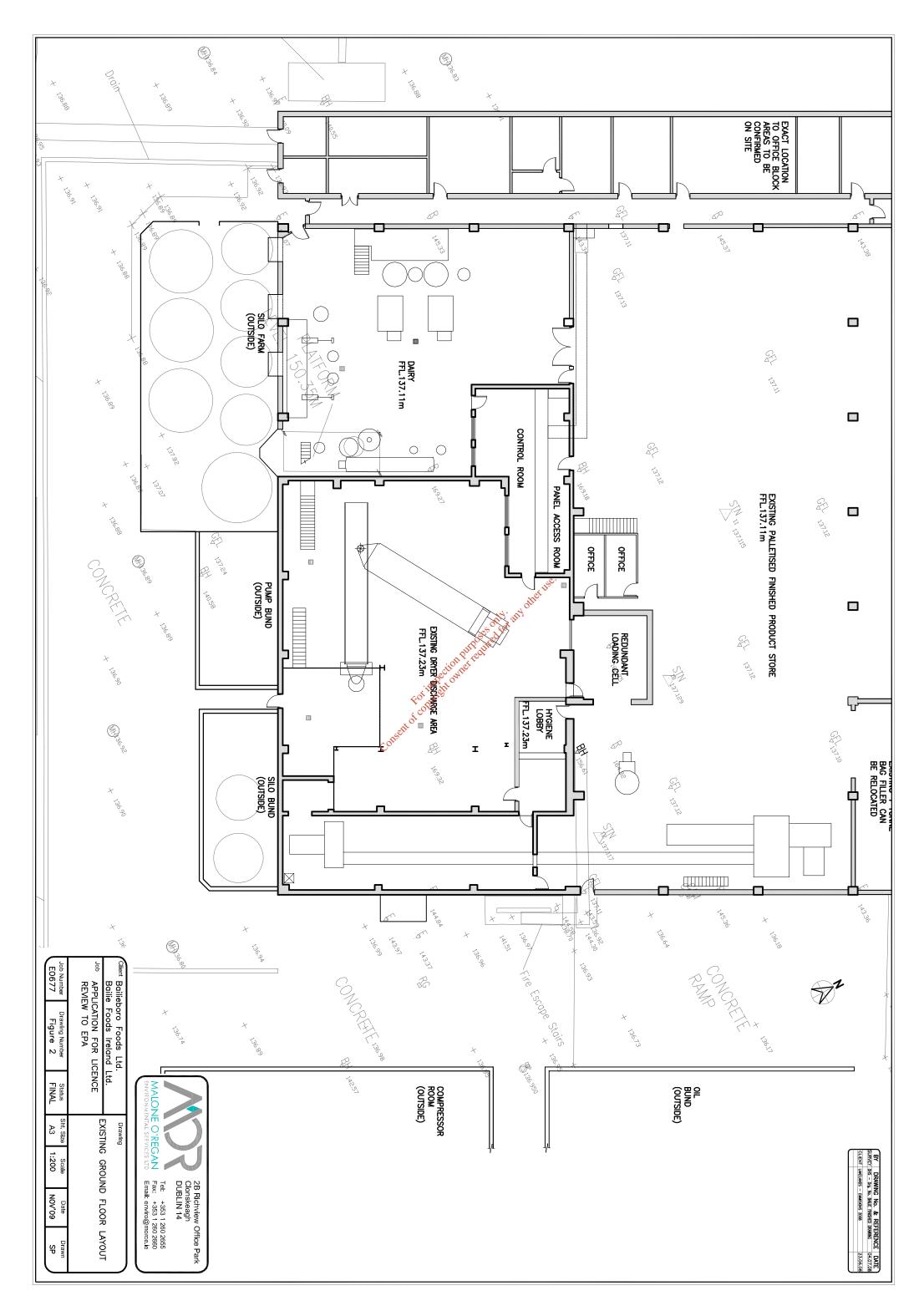
<u>CCP Reference for process flow step numbers:</u>

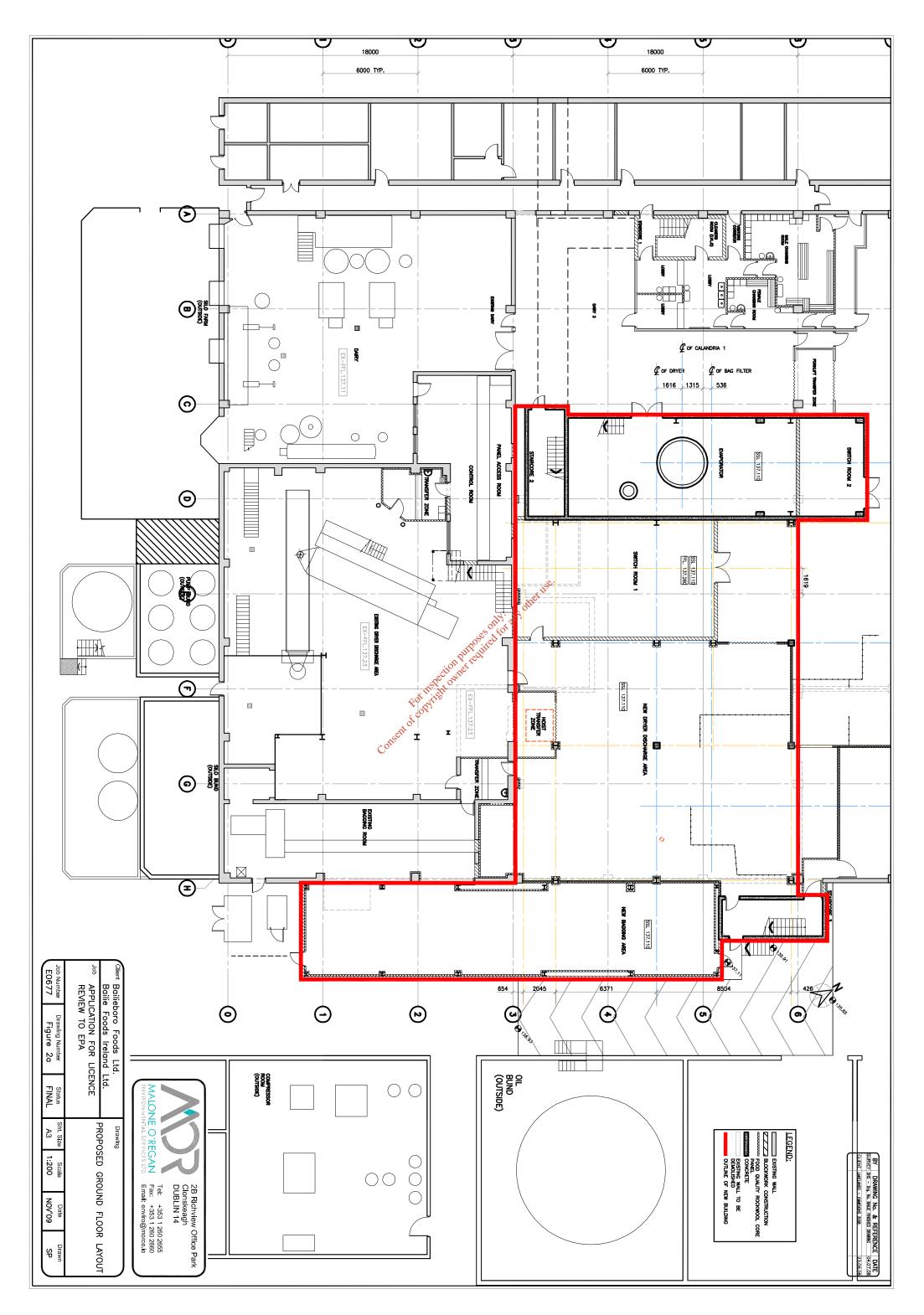
Step No.	CCP No.	Control measure			
Creamery Process	Creamery Process				
1A	CCP 1	Antibiotic MRL			
2A	CCP 1	Antibiotic MRL			
3A	CCP 2	Filter – Final control for milk for dispatch			
10A	CCP 3	Pasteurisation			
19A	CCP 3	Pasteurisation			
24A	CCP 3	Pasteurisation			
25A	CCP 3	Pasteurisation			
26A	CCP 2	Filter - Final control for cream for dispatch			
Butter Process 25Kg					
1B	CCP 2	Filter			
10B	CCP 2	Filter			
12B	CCP 2	Filter			
21B	CCP 2	Filter			
30B	CCP 4	Metal detection			
Butter Process 250g		e.			
1C	CCP 2	Filter			
10C	CCP 2	Theorem and the second se			
22C	CCP 4	Metal detections			
Drying Process		all			
2D	CCP 1	Antibiotic MRL			
6D	CCP 3	Heattreatment			
10D	CCP 3 CCP 5 For star	Heat treatment			
25D	CCP 5 FOR	Sieves 1 & 2			
25D CCP 5 Sieves 1 & 2 Powder Packing Process Sieves 1 & 2					
15E	CCP 4 sent	Metal detection			
21E	CCF ⁴	Metal detection			

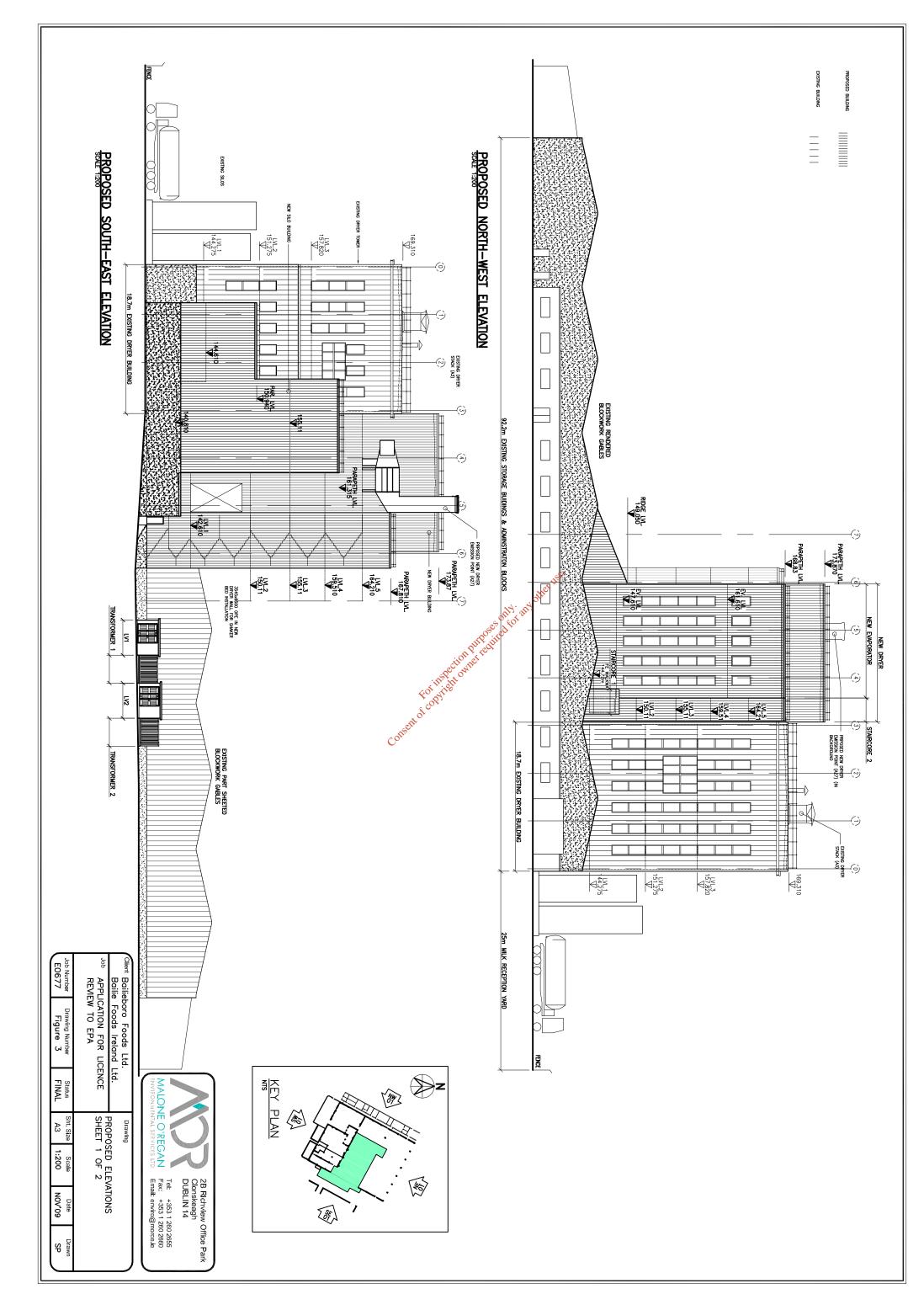
Bailieboro Foods Ltd. and Bailie Foods Ireland Ltd.

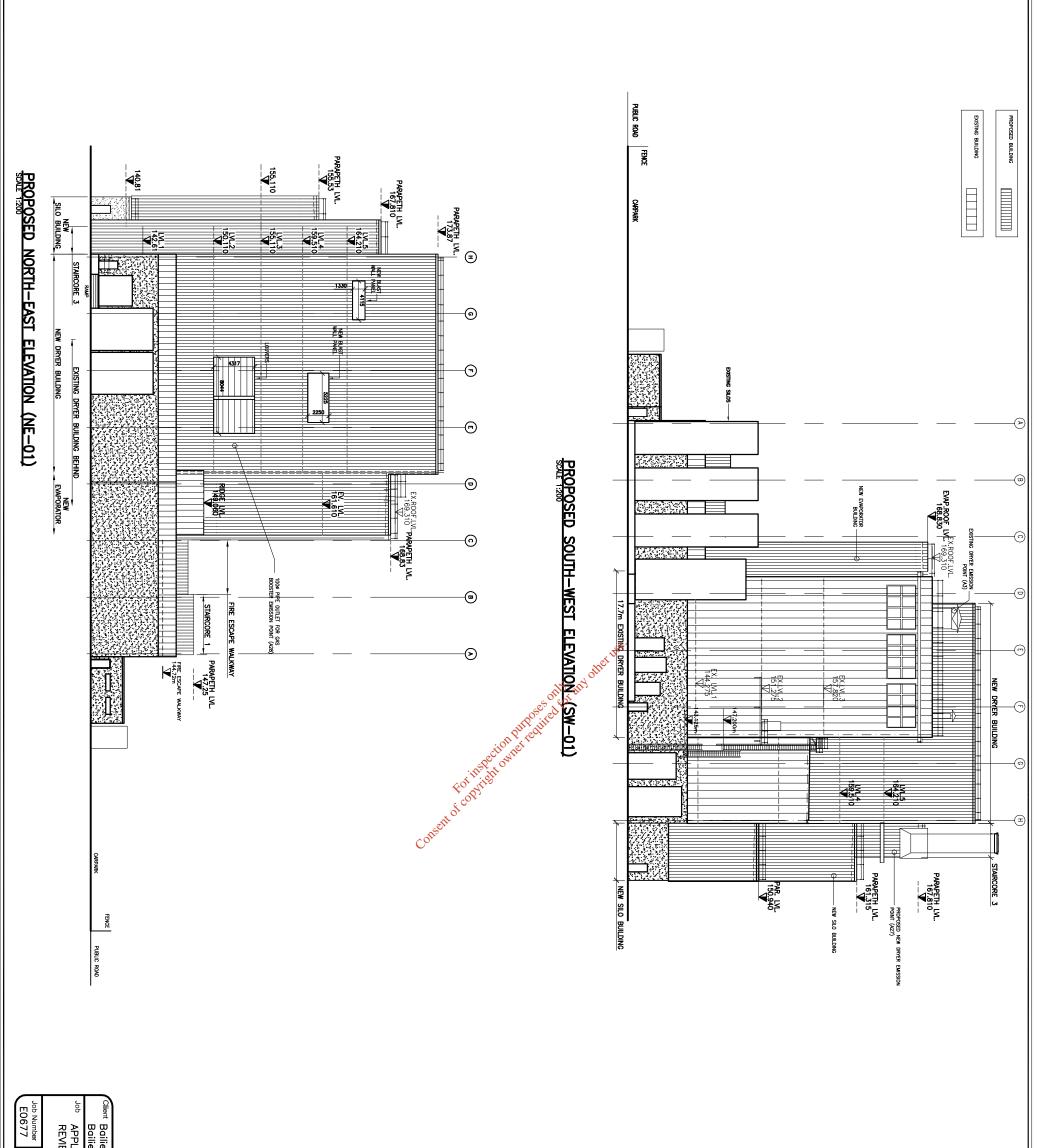




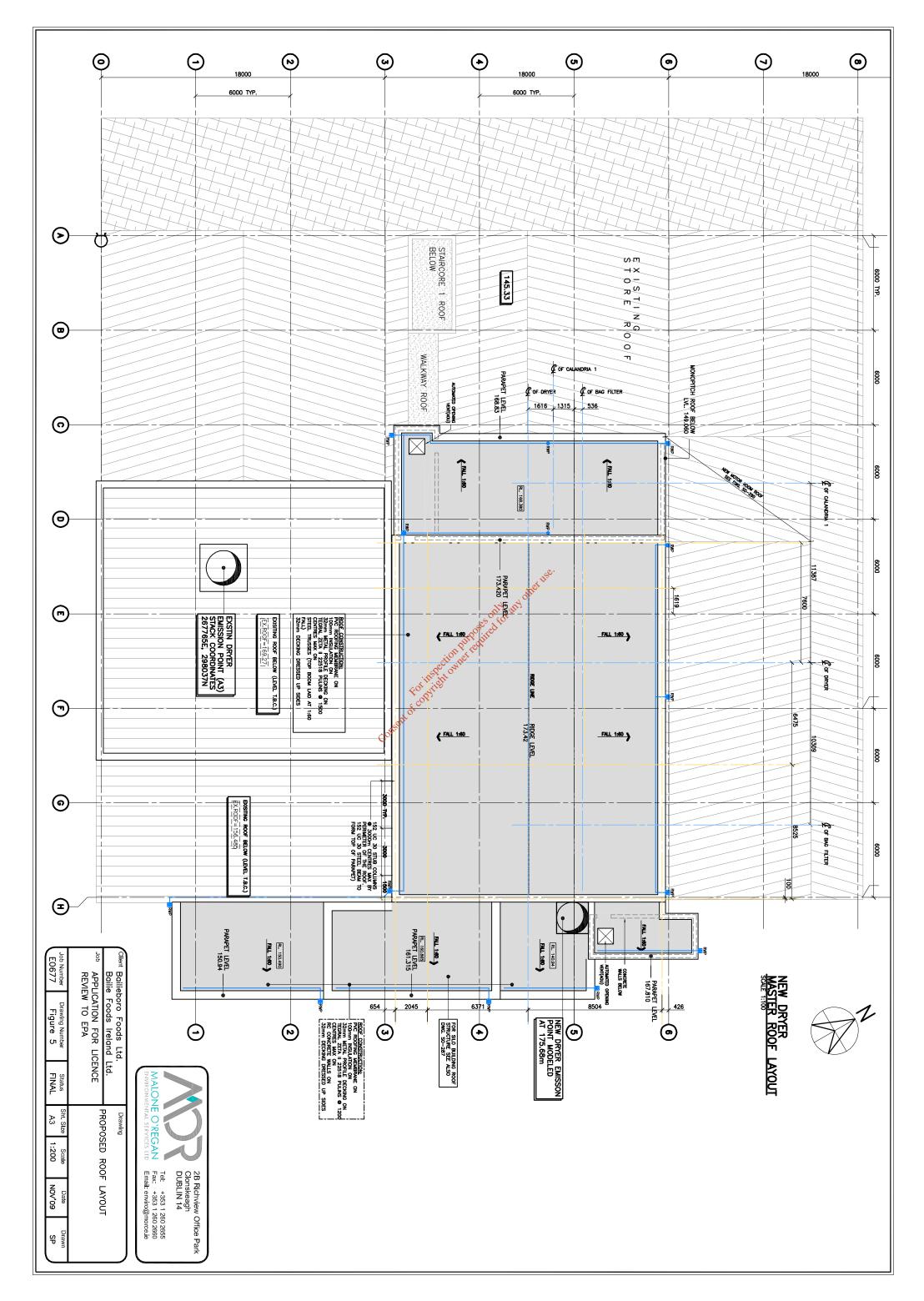


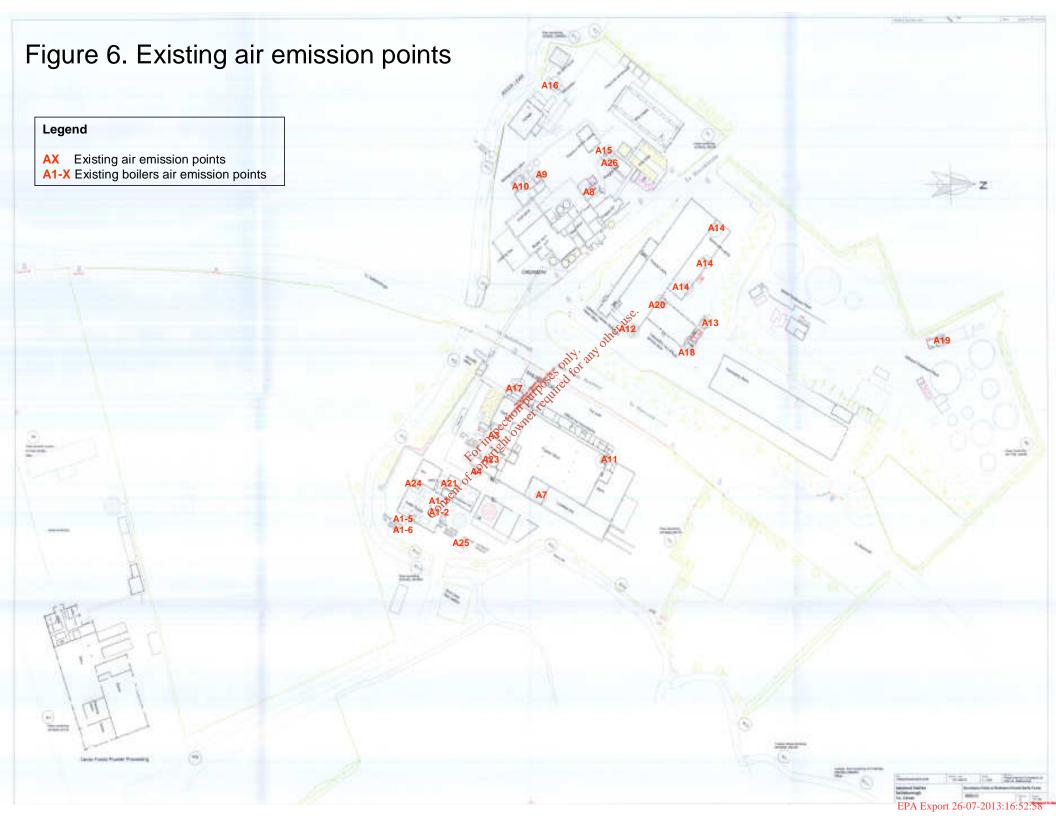


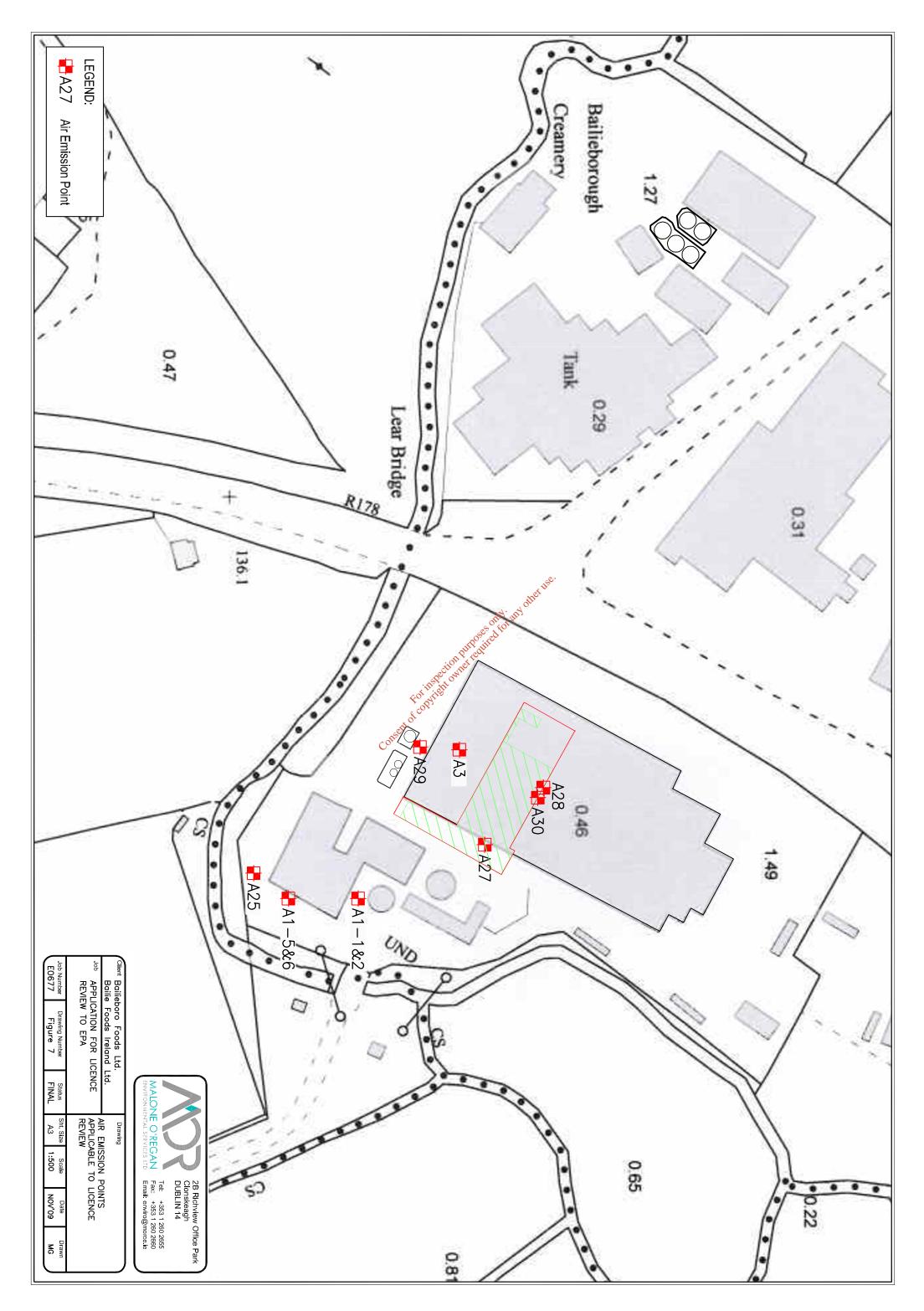




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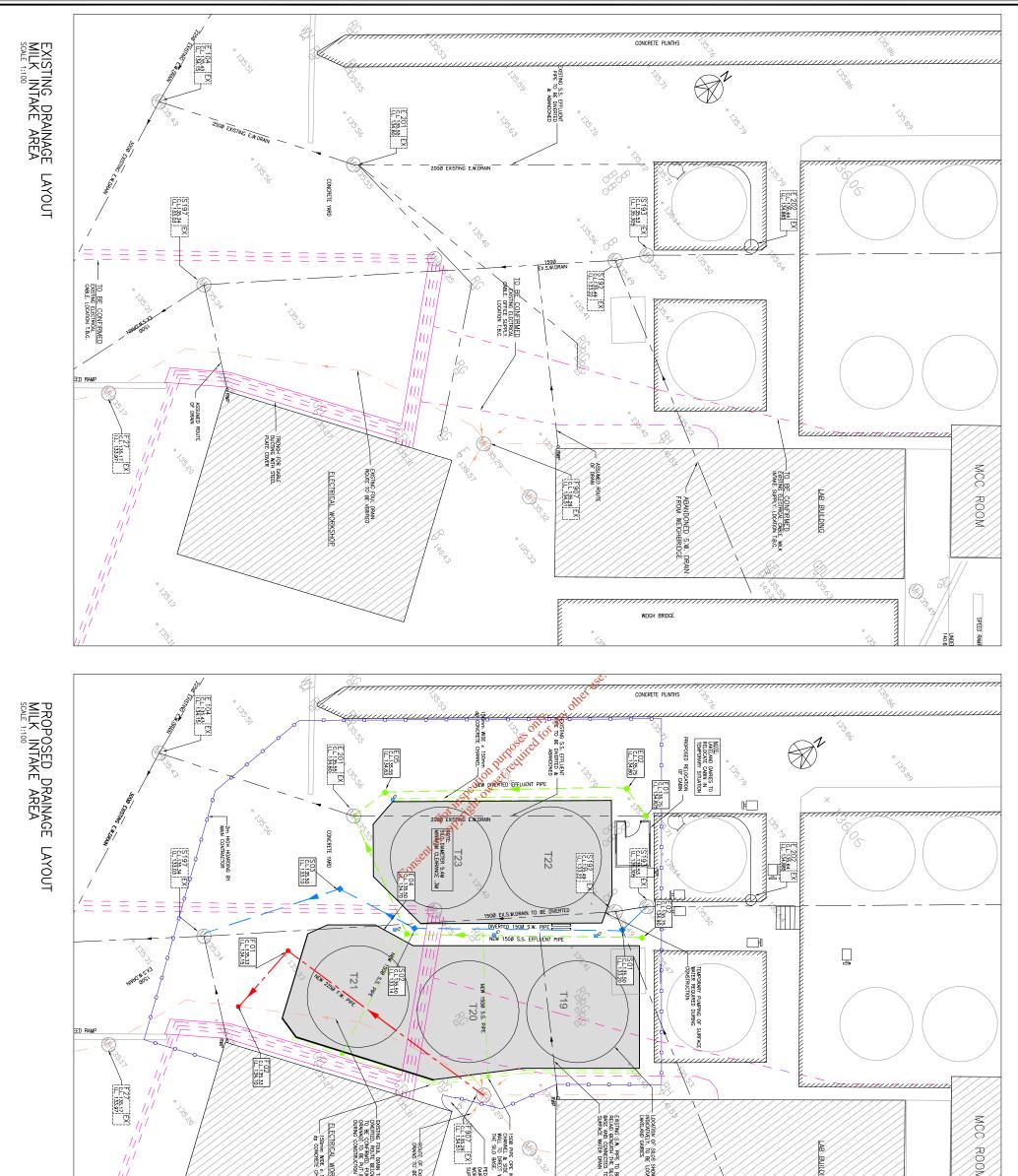
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